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MIXED CONVECTION FLOWS OF TANGENT HYPERBOLIC FLUID PAST AN ISOTHERMAL WEDGE WITH ENTROPY: A MATHEMATICAL STUDY

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ABSTRACT

The non-linear, steady, mixed convective boundary layer flow and heat transfer of an incompressible tangent hyperbolic non-Newtonian fluid from an isothermal wedge in the presence of magnetic field is analyzed numerically using the Keller Box implicit finite difference technique. The entropy analysis due to MHD flow of tangent hyperbolic fluid past an isothermal wedge and viscous dissipation is also included. The numerical code is validated with previous Newtonian studies available in the literature. Graphical and tabulated results are analyzed to study the behavior of fluid velocity, temperature, concentration, shear stress, heat transfer rate, entropy generation number and Bejan number for various emerging thermo physical parameters, namely, Weissenberg number (We), power law index (n), mixed convection parameter (λ), pressure gradient parameter (m), Prandtl number (Pr), Biot number (γ), Hartmann number (Ha), Brinkmann number (Br), Reynolds number (Re) and temperature gradient (Π). It is observed that velocity, entropy, Bejan number and surface heat transfer rate are reduced with increasing Weissenberg mamber, but temperature and local skin friction are increased. Increasing pressure gradient enhances velocity, entropy, local skin friction and surface heat transfer rate but reduces temperature and Bejan number. An increase in an isothermal power law index (n) is observed to increase velocity, Bejan number and surface heat transfer rate but decreases temperature, entropy and local skin friction. Increasing magnetic parameter (Ha) is found to decrease temperature, entropy, surface heat transfer rate and local skin friction and increases velocity and Bejan number. The research is applicable for coating materials in chemical engineering for instance, robust paints, production of aerosol deposition and water soluble solution thermal treatment.

KEYWORDS: Tangent Hyperbolic fluid; Weissenberg mumber; power law index; Hartmann mumber; Mixed Convection; pressure gradient parameter; ...

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NOMENCLATURE

Bo	externally imposed radial magnetic field		Greek Symbols
Ве	Dimensionless Bejan number	α	Thermal diffusivity
Br	Brinkmann number	β	The coefficient of thermal expansion
C	Positive constant	Ω	Wedge angle
C_f	Skin Friction Coefficient	σ	Electric conductivity of the fluid
f	Dimensionless stream function	η	Non-dimensional radial coordinate
g	Gravitational acceleration	μ	Dynamic viscosity
Gr_{x}	Local Grashof number	Š	Non-dimensional tangential coordinate
На	Hartmann number (magnetic parameter)	Ψ	Non-dimensional stream function
h_w	convective heat transfer coefficient	ν	Kinematic viscosity
k	Thermal conductivity of the fluid	Γ	Time dependent material constant
m	Pressure gradient	θ	Dimensionless temperature
n	Power law index i.e. flow behavior index	ρ	Fluid density
Ng	Entropy generation number	П	Second invariant strain tensor
Nu	Heat transfer coefficient	μ_{∞}	infinite shear rate viscosity
Pr	Prandtl number	γ	Biot number
Re_x	Reynolds Number	τ	extra stress tensor
T	Fluid temperature	П	Temperature gradient
$T_{\rm w}$	Convective fluid temperature	β_l	Total angle of the wedge
U_{∞}	Free steam velocity	λ	Mixed convection parameter
u, v	Dimensionless velocity components in X and Y direction respectively	μ_0	zero shear rate viscosity
V	Velocity vector	ÿ	shear rate
We	Local Weissenhere number		Subscripts
	_	w	
		00	
We x y	Local Weissenberg number Stream wise coordinate Transverse coordinate		Subscripts Conditions on the wall Free stream condition

INTRODUCTION

Due to constantly new advances in technology and engineering, non-Newtonian liquids became an issue of considerable interest to researchers for over past few decades. Sources of these fluids comprise coal-oil slurries, detergents, pain, smart coatings and suspension, grease. Cosmetics, custard, biological liquids, etc. The non-Newtonian fluids constitutive equations can never be characterized with one constitutive relation involving rate of strain and stress like the viscous (Newtonian) fluids. These fluids have complex attributes in nature and industry. Generally, the mathematical model of the non-Newtonian liquids is complex due to the significant nonlinearity and higher order differential transportation equations especially as compared to viscous fluids. Considering their complications, researchers are involved in dynamics of non-Newtonian liquids as such fluids have wide applications in biotechnological production, plastic manufacturing, medical sciences, etc. Though the system of equations evolving in non-Newtonian fluids typically need access to numerical techniques, in some restricted cases closed form analytical solutions were achieved. Fetecau et al. [1] presented the Caputo-Fabrizio's concept of nonlinear systems to obtain appropriate solution for second-grade hydromagnetic movement of fluids past a moving infinite flat plate. Geethan et al. [2] considered the 3D hydromagnetic chemically radiative flows of Jeffery's fluid past the stretchable porous surface considering the effects of heat source/sink and Soret number. Shehzad et al. [3] under the implications of thermophoresis and the Cattaneo-Christov principle conducted the numerical study of Maxwell fluid flows past revolving disk. Panchun et al. [4] studied the rotational electro-osmotic flow of Oldroyd-B fluid in a microchannel. They also considered the Oldroyd-B fluid's viscoelasticity and slip effect on electroosmotic flow velocity distributions. Ijaz et al. [5] discussed the Carreau fluid's stagnation point MHD flows past a stretching and shrinking cylindrical surface. Meenakumari and Lakshminarayana [6] employed shooting technique to investigate the unsteady chemically radiative MHD 3D Williamson fluid flow past a stretching surface considering the effects of Hall current and heat source/sink. Sayer et al. [7] discussed the entropy generation of MHD thermally radiative Eyring-Powell fluid through an unstable oscillating porous stretchable surface. Das et al. [8] examined the impact of Soret and variable heat absorption on unsteady chemically radiative MHD flows of Casson fluid through a stretchable porous surface. Chamkha et al. [9] investigated the entropy generation of MHD mixed convective nanofluid flows in a Gamma shaped porous cavity.

The Tangent Hyperbolic fluid is a four-constant fluid model, designed to explain the shear thinning characteristics, is amongst the non-Newtonian constitutive models that have arisen [10] [11]. This Tangent Hyperbolic fluid model has many applications in chemical engineering and it does have few benefits over many various non-Newtonian liquid models. It has be observed in lab experiments that the present model accurately describes the blood flows. The tangent hyperbolic fluid is a rate type fluid model that describes the attributes of relaxation and the retardation times. This model represents the viscosity depending on shear rate as a mathematical hyperbolic tangent function. The apparent viscosity of such fluids steadily varies from zero shear rate to infinity shear rate. Few prime examples of such fluid include, magma, ketchup, whipped cream, blood, sprays coating and so on. Using the hyperbolic tangent model, calendaring, which is a continuous production activity for thermoplastic sheets or films of uniform thickness accomplished via a pair of heated driven rolls of equal or unequal diameters, was simulated by Kiparissides and Vlachopoulos [12]. Magnetohydrodynamics abbreviated as MHD, is the study of extremely electrically conductive fluids with magnetic characteristics. The electrically induced fluid flows all over the magnetic field and current generates and hence the flow and the magnetic field effects variate. In various fields such as oil and natural gases, atmospheric sciences, agricultural production, geosciences, solar and astro physics, MHD plays a leading role. Examples of magento liquids inclue electrolytes, sea water, oil metals and plasma. Zakir et al. [10] presented the Lie group analysis of an incompressible tangent-hyperbolic fluid MHD convection considering the velocity and thermal slip effects along with suction/injection effects. Ovelakin and P. Sibanda [13] analyzed the importance of variable viscosity and thermal conductivity in tangent-hyperbolic MHD flows. Veera and Chamkha [14] addressed the impacts of Dufor, radiation and heat generation on MHD convection Nanofluid flows past a semi-infinite porous plate considering the Hall and Ionslip effects. Kumar et al [15] examined the MHD mixed convection flows of optically thin fluid past a vertical plate considering the radiation and dissipation effects. Mamata et al. [16] employed the shooting technique to explore the impacts of heat source on chemically radiative MHD flows of tangent-hyperbolic liquid past an exponentially expanding sheet. Farooq et al. [17] examined the slip and chemical reaction effects on peristalsis of tangent hyperbolic fluid in a curved channel. Ganesh et al. [18] proposed the thermally radiative MHD flows of tangent hyperbolic fluid over a stretching sheet with suspension of the fluid particles. Jitendra et al. [19] investigates the effects of Hall current on MHD mixed convection flows of viscoelastic fluid past

vertical surface using the perturbation technique. Venkatadri et al. [21] theoretically presented the radiative MHD nanofluid flows across a progressively stretching/shrinking permeable surface with melting. Aziz et al. [21] presented the rheological characteristics of 3D couple stress chemically radiative nanofluid MHD flows induced by oscillating stretchable surface.

Falkner-Skan flows [22] have been considered by very few researchers. The 2D wedge design is connected with this family of boundary layer flows. Non-Newtonian flows past wedge geometries emerge in various chemical engineering fields using the second-order Reiner-Rivlin model. A significant attention has been drawn towards the mixed convection boundary layer flux past a wedge. In the presence of thermal radiation with a Rosseland diffusion approximation, a non-similar solution of mixed convection flow of a Nanofluid past an isothermal wedge immersed in a permeable porous medium was examined by Chamkha *et al.* [23]. Takhar *et al.* [24] discussed in the presence of magnetic field, the unsteady mixed convection flow over a rotating vertical cone. Gorla *et al.* [25] analyzed the mixed convection boundary layer flows of Nanofluid past a vertical wedge immersed in a permeable porous medium. Thameem *et al.* [26] reported the forced convection Falkner-Skan flow of a single walled carbon NanoHorn and water Nanofluid past a wedge, plate and stagnation point in the presence of nonlinear radiation and induced magnetic field. Chamkha *et al.* [27] explored the radiative mixed convection boundary layer flow of Nanofluid past a vertical cone immersed in a porous media.

Convective heat transfer has generated significant attention due to its significance in energy and biological innovations like power generation, diesel generators, nuclear power plants, missile technology, hydroelectric reserves, photovoltaic systems etc. Also, the convective boundary condition has fascinated considerable attention and is typically synchronized in the thermal boundary condition of the wall via a Biot number. Nurul et al. [28] examined the MHD mixed convection stagnation point flow of hybrid nanofluid through a vertical flat plate with convective boundary condition. Hayat et al. [29] dealt with the impact of binary chemical reaction and activation energy in third grade nanofluid hydromagnetic flow combined with convective boundary condition via non-linearly stretched sheet. Najiyah et al. [30] discussed the impacts of velocity slip and convective boundary condition on 3D hybrid nanofluid flow past a stretching/shrinking surface. Rai et al. [31] analyzed the heterogeneous and homogeneous effects on the viscous fluid flow past a non-linear shaped stretchable surface with convective heating mechanism. Patel and Rajiv [32] studied the computational modelling of chemically radiative

MHD mixed convection flows of microplar fluid past non-linear stretching surface embedded in porous media considering the effects of viscous dissipation, Joule heating and convective boundary condition. Sudarsana et al. [33] examined the heat flow behavior of nanofluid past a vertical cone embedded in porous media considering the effects of magnetic field, thermal radiation and chemical reaction of first order due to convective boundary condition. Gajjela and Garvandha [34] considered the MHD free convection flow, double-diffusion couple stress fluid past a stretching cylinder with surface imposed Robin boundary condition.

In thermodynamics, entropy is the sum of inaccessible energy in the process. Entropy refers to irreversibility of the device and the concept is widely seen in thermodynamics architecture. High entropy decreases the usable energy and has a significant effect on the efficiency of the device. Entropy demonstrates the means of separating the real materials through its components. In the irreversible processes, the initial state of the process and nearby environment cannot be preserved. Entropy and irreversibility analysis are directly proportional. Also, entropy tells us how the energy is utilized. The process is flexible due to the difference in temperature which induces energy transfer. The gradient of the system stimulates irreversibility to the process. Entropy leads to an increase in disorder in process which induces energy loss in the system and leads to a reduction in work potential. Thus, as we process the system, we restrict entropy generation and it is critical in various engineering applications, one of which is the power generation in power plants. Many researchers are focused on various approaches for entropy minimization in fluid flow problems. Bejan [28, 29] was the first to propose entropy generation minimization (EGM) to measure the disorders in isolated system. Rashad et al. [37] employed finite volume technique to investigate the entropy analysis and MHD mixed convection flow of Nanofluid in a lid driven U-shaped cavity with heat source. Mansour et al. [38] discussed the entropy generation and MHD mixed convection flow of Nanofluid in a C-shaped cavity with a corner heater and heat source. Chamkha et al. [39] presented the entropy generation analysis on MHD mixed convection flows of Nanofluid past a porous enclosure considering the effects of heat source/sink. Armaghani [40] studied the analytical simulation of thermal efficiency using entropy generation of MHD mixed convection flow of Nanofluid in an L-shaped duct using finite volume method. Fatunmbi and Adeniyan [41] reported the entropy generation and irreversibility analysis of nonlinearly radiative MHD micropolar fluid flow past a non-linear and non-permeable stretching surface using RK technique considering the effects of Joule heating and viscous dissipation. Li et al. [42] analyzed the entropy generation of radiative MHD nanofluid in a square cavity. Zafar et al. [43] presented the entropy generation of triple diffusive flow past a horizontal plate. Armaghani et al. [44] investigated the entropy generation in a porous I shaped cavity owing to MHD convection of Nanofluid in the presence of heat generation/absorption using finite difference technique.

There has been several literature reports in numerous perspectives relating to the dynamics of Tangent Hyperbolic liquid through an isothermal wedge. But as per the authors knowledge the non-similar solutions of Tangent Hyperbolic fluid past an isothermal wedge flows has not been considered. Therefore, the objective of the present study is to examine the MHD flow and heat transfer of tangent hyperbolic fluid through an isothermal wedge with convection boundary condition. Appropriate non-similar transformations are deployed to render the conservation equations dimensionless. The emerging non-dimensional partial differential equations with associated dimensionless boundary conditions constitute a highly nonlinear, coupled two-point boundary value problem making exact solutions practically impossible. The transformed dimensionless equations with appropriate boundary conditions are solved using the Keller's box implicit finite difference technique [45]. The impacts of various thermo-physical parameters, namely local Weissenberg number (We), local magnetic parameter (Ha), local biot number (?), mixed convection parameter (λ), pressure gradient parameter (m) and Prandtl number (Pr) on velocity, temperature, shear stress, entropy generation number, Bejan number and heat transfer rate are presented both graphically and numerically. The research is applicable for coating materials in chemical engineering for instance, robust paints, production of aerosol deposition and water soluble solution thermal treatment.

TANGENT HYPERBOLIC FLUID MODEL

Due to its simplicity, the current work employs a subclass of non-Newtonian fluids called the tangent hyperbolic fluid. The Cauchy stress tensor for a tangent hyperbolic fluid [10-11] is:

$$\overline{\tau} = \left[\mu_{\infty} + (\mu_0 + \mu_{\infty}) \tanh \left(\Gamma \dot{\gamma} \right)^n \right] \overline{\dot{\gamma}}$$
(1)

where the shear rate, \dot{y} is defined as:

$$\gamma = \sqrt{\frac{1}{2} \sum_{i} \sum_{j} \gamma_{ij} \gamma_{ji}} = \sqrt{\frac{1}{2} \Pi}$$
(2)

Here $\Pi = \frac{1}{2} tr \left(gradV + \left(gradV \right)^T \right)^2$. We consider the case where $\mu_{\infty} = 0$ as numerical computations are not possible at infinite shear rate viscosity. Moreover, we confine to tangent hyperbolic fluid that describes shear thinning effects, *i.e.*, $\Gamma \dot{\gamma} < 1$. Taking these assumptions into consideration, Eqn. (1) can be written as,

$$\overline{\tau} = \mu_0 \begin{pmatrix} \overline{\tau} \\ \overline{\tau} \end{pmatrix}^n = \mu_0 \begin{bmatrix} \overline{\tau} \\ 1 + \overline{\tau} \\ \overline{\tau} - 1 \end{pmatrix}^n = \mu_0 \begin{bmatrix} 1 + n \begin{pmatrix} \overline{\tau} \\ \overline{\tau} \\ \overline{\tau} - 1 \end{pmatrix} = \mu_0 \begin{bmatrix} \overline{\tau} \\ \overline{\tau} \\ \overline{\tau} - 1 \end{bmatrix} = \mu_0 \begin{bmatrix} \overline{\tau} \\ \overline{\tau} \\ \overline{\tau} \\ \overline{\tau} - 1 \end{bmatrix} = \mu_0 \begin{bmatrix} \overline{\tau} \\ \overline{\tau} \\$$

MATHEMATICAL MODEL

An incompressible, steady, laminar mixed convection flow of tangent hyperbolic fluid over an isothermal wedge with convective boundary condition and magnetohydrodynamic is examined. The physical schematic diagram of the problem is illustrated in Fig. 1. The x (streamwise) and y (transverse) coordinates are considered along the wedge and normal to the surface respectively. The gravitational acceleration, g is considered to act downwards. A uniform magnetic field of strength B_0 is applied parallel to the y-axis i.e. transverse to the wedge surface. Magnetic induction, Hall current, ionslip and Maxwell displacement currents are neglected. Magnetic Reynolds number is small and the electric field due to polarization of charges is negligible. Both the fluid and wedge surface are initially held at a fixed temperature. Additionally, the electron pressure (for weakly conducting fluids) and the thermo-electric pressure are neglected. The applied magnetic field, B_0 , is generated by passing a steady electric current along the longitudinal (z-axis) parallel to the cone, where the wedge edges terminate at perfect electrodes which are connected via a load. Further, under usual boundary layer and Boussinesq approximations, the relevant equations for mass, linear momentum and energy are as follows:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{4}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = U_{\infty}\frac{dU_{\infty}}{dx} + v(1-n)\frac{\partial^{2}u}{\partial y^{2}} + \sqrt{2}vn\Gamma\left(\frac{\partial u}{\partial y}\right)\frac{\partial^{2}u}{\partial y^{2}} \pm g\beta\sin\left(\frac{\Omega}{2}\right)(T-T_{\infty}) - \frac{\sigma B_{0}^{2}}{\rho}u$$
 (5)

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} \tag{6}$$

The non-Newtonian impacts only display in the shear terms in eqn. (5) and not in the convection term, though they often make the fluid dynamics quite intensely non-linear relative to the Newtonian fluids.

At
$$y = 0$$
, $u = 0$, $v = 0$, $-k\frac{\partial T}{\partial y} = h_w(T_w - T)$
As $y \to \infty$, $u \to U_m = Cx^m$, $T \to T_m$ (7)

Here
$$m = \frac{\beta_1}{2 - \beta_1}$$
 and $\beta_1 = \frac{\Omega}{\pi}$. The stream function Ψ is defined as $u = \frac{\partial \psi}{\partial y}$ and $v = -\frac{\partial \psi}{\partial x}$.

Consequently, Eqn. (4) is satisfied. The following dimensionless quantities are adopted:

$$\xi = \frac{\sigma x}{\rho U_{\infty}}, \quad \eta = \frac{y}{x} \operatorname{Re}_{x}^{1/2}, \quad \psi = \left(U_{\infty} x v\right)^{1/2} f, \quad \theta = \frac{T - T_{\infty}}{T_{w} - T_{\infty}}, \quad \operatorname{Re}_{x} = \frac{U_{\infty} x}{v}$$
(8)

In the light of Eqn. (8), the governing equations (5) – (7) can be written as:

$$(1-n)f''' + \left(\frac{1+m}{2}\right)ff''' + nW_ef'''f''' + m\left(1-\left(f'\right)^2\right) - Haf' + \lambda\theta\sin\left(\frac{\Omega}{2}\right) = \xi\left(1-m\right)\left(f'\frac{\partial f'}{\partial \xi} - f''\frac{\partial f}{\partial \xi}\right)$$

$$(10)$$

$$\frac{\theta''}{\Pr} + \left(\frac{1+m}{2}\right)f\theta' = \xi(1-m)\left(f'\frac{\partial\theta}{\partial\xi} - \theta'\frac{\partial f}{\partial\xi}\right) \tag{11}$$

The transformed dimensionless boundary conditions are:

At
$$\eta = 0$$
, $f = 0$, $f' = 0$, $\theta = 1 + \frac{\theta'}{\gamma}$

As $\eta \to \infty$, $f' \to 0$, $\theta \to 0$ (12)

Here

$$\gamma = \frac{xh_{w} \operatorname{Re}_{x}^{1/2}}{k}$$
, $\operatorname{Pr} = \frac{v}{\alpha}$, $Gr_{x} = \frac{g\beta_{1}(T_{w} - T_{\infty})x^{3}}{v^{2}}$, $We = \frac{\sqrt{2}v\Gamma \operatorname{Re}_{x}^{3/2}}{x^{2}}$, $\lambda = \frac{Gr_{x}}{\operatorname{Re}^{2}}$ and $Ha = B_{0}^{2}x^{2}\frac{\sigma}{u}$

Due to non-similar nature of the flow, the parameters We, Gr_x , γ and Ha are local i.e., they are function of the tangential coordinate x. The thermal boundary condition at the wall in Eqn. (12)

refers to the convective cooling. The shear stress rate and heat transfer rate at the wedge surface are defined as:

$$\operatorname{Re}_{x}^{V2} C_{f} = (1-n) f''(\xi, 0) + \frac{n}{2} W_{e} [f''(\xi, 0)]^{2}$$
(13)

$$\operatorname{Re}_{x}^{1/2} Nu = -\theta'(\xi, 0)$$
 (14)

ENTROPY ANALYSIS

The entropy analysis for the present flow regime in line with Bejan [35] is considered in this section. The volumetric rate of entropy generation due to magnetic field with heat transfer is given as:

$$S_{gen}^{*} = \frac{k}{T_{\infty}^{2}} \left(\frac{\partial T}{\partial y}\right)^{2} + \frac{\mu}{T_{\infty}} \left((1-n) + \frac{n\Gamma}{\sqrt{2}} \frac{\partial u}{\partial y}\right) \left(\frac{\partial u}{\partial y}\right)^{2} + \frac{\sigma B_{0}^{2} u^{2}}{T_{\infty}}$$
(15)

The first term in eqn. (15) signifies the entropy generation produced by heat transfer, the second term denotes the entropy generation due to fluid friction and the third term is the entropy generation due to the magnetic Lorentz force. The non-dimensional entropy heat generation (Ng) is defined as:

$$Ng = \frac{S_{gen}^{-}}{S_{0}^{-}} = \left(\frac{\frac{k}{T_{\infty}^{2}} \left(\frac{\partial T}{\partial y}\right)^{2} + \frac{\mu}{T_{\infty}} \left((1-n) + \frac{n\Gamma}{\sqrt{2}} \frac{\partial u}{\partial y}\right) \left(\frac{\partial u}{\partial y}\right)^{2} + \frac{\sigma B_{0}^{2} u^{2}}{T_{\infty}}}{\frac{k(\Delta T)^{2}}{x^{2} T_{\infty}^{2}}}\right)$$
(16)

$$Ng = \operatorname{Re}_{x} \theta^{12} + \frac{Br}{\Pi_{1}} \operatorname{Re}_{x} (1 - n) f^{112} + \frac{nWe^{2}}{2} \frac{Br}{\Pi_{1}} \operatorname{Re}_{x} f^{113} + \frac{Br}{\Pi_{1}} Ha f^{12}$$
(17)

Here
$$Br = \frac{\mu u_{\infty}^2}{k \Delta T}$$
, $Ha = B_0^2 x^2 \frac{\sigma}{\mu}$, $\Pi_1 = \frac{\sigma}{\mu}$ and $Re_x = \frac{U_{\infty} x}{\nu}$.

The Bejan number (Be) is defined as the ratio of entropy heat generation due to heat and mass transfer to the overall entropy heat generation i.e.:

$$Be = \frac{Entropy due to Heat transfer}{Total entropy}$$
 (18)

NUMERICAL SOLUTION WITH IMPLICIT KELLER BOX METHOD (KBM)

The non-dimensional Eqns. (10) – (12) form a 5th order non-linear boundary value problem that needs a numerical solution. To solve this system of equations we implement the implicit finite differences scheme proposed by Keller known as Keller-Box Technique [45]. This approach remains highly popular and has retained comparative reliability than other numerical techniques. However, the drawback of this method is that because of its step, which must substitute the higher derivative with the first derivative, the computational effort per time step is costly, so that the second order derivatives can be written as a system of two first order derivatives. The discretized equations produce laborious algebraic expressions. The KBM however, has a second order accuracy with arbitrary spacing and appealing extrapolation characteristics. This method is very stable and outstanding precision is achieved. It converges easily and offers numerical meshing functions that are secure. The KBM offers an increase in the consistency of explicit or semi-implicit frameworks and uses a completely implicit methodology. For further details the readers can refer to [46] – [50]. The present KBM solutions are validated with the previous Newtonian computations. KBM comprises of the following 4 steps:

- Reduction of Nth order partial differential system to N first order differential equations.
- Finite difference discretization.
- Newton quasilinearization of non-linear Keller algebraic equations.
- Block-Tridiagonal elimination of Keller algebraic equations.

Step1: Reduction of the Nthorder partial differential equation system to N first order equations. New variables are introduced to Eqns. (10)-(12), to render the boundary value problem as a multiple system of first order equations. A set of five simultaneous first order differential equations are therefore generated by introducing the new variables:

$$u(x, y) = f', v(x, y) = f'', s(x, y) = \theta, t(x, y) = \theta'$$
(19)

$$f' = u$$
 (20)

$$u' = v$$
 (21)

$$s'=t$$
 (22)

$$(1-n)v' + \frac{1+m}{2}fv + nWevv' + (1-u^2)m + \lambda\sin(\Omega)s - Hau = \xi(1-m)\left[u\frac{\partial u}{\partial \xi} - v\frac{\partial f}{\partial \xi}\right]$$
 (23)

$$\frac{t'}{\Pr} + \frac{1+m}{2}f = \xi(1-m)\left(u\frac{\partial s}{\partial \xi} - t\frac{\partial f}{\partial \xi}\right)$$
(24)

where primes denote differentiation with respect to η . In terms of the dependent variables, the boundary conditions become:

At
$$\eta = 0$$
, $f = 0$, $u = 0$, $s = 1$
As $\eta \to \infty$, $u \to 0$, $s \to 0$ (25)

Step 2: Finite Difference Discretization

A two-dimensional computational grid is imposed on the ξ - η plane as sketched in Fig. 2. The stepping process is defined by:

$$\eta_0 = 0, \quad \eta_j = \eta_{j-1} + h_j, \quad j = 1, 2, ..., J, \quad \eta_J \equiv \eta_{\infty}$$
 (26)

$$\xi^{0} = 0, \quad \xi^{n} = \xi^{n-1} + k_{n}, \quad n = 1, 2, ..., N$$
 (27)

where k_n is the $\Delta \xi$ -spacing and h_j is the $\Delta \eta$ -spacing. If g_j^n denotes the value of any variable at (η_j, ξ^n) , then the variables and derivatives of Equations (20) – (24) at $(\eta_{j-1/2}, \xi^{n-1/2})$ are replaced by:

$$g_{j-1/2}^{n-1/2} = \frac{1}{4} \left(g_j^n + g_{j-1}^n + g_j^{n-1} + g_{j-1}^{n-1} \right) \tag{28}$$

$$\left(\frac{\partial g}{\partial \eta}\right)_{j-1/2}^{n-1/2} = \frac{1}{2h_j} \left(g_j^n - g_{j-1}^n + g_j^{n-1} - g_{j-1}^{n-1}\right)$$
(29)

$$\left(\frac{\partial g}{\partial \zeta}\right)_{j-1/2}^{n-1/2} = \frac{1}{2k^n} \left(g_j^n - g_{j-1}^n + g_j^{n-1} - g_{j-1}^{n-1}\right)$$
(30)

The resulting finite - difference approximation of equations (20) – (24) for the mid - point $(\eta_{j-1/2}, \xi^n)$, are:

$$h_i^{-1}(f_i^n - f_{i-1}^n) = u_{i-1/2}^n$$
 (31)

$$h_i^{-1}(u_i^n - u_{i-1}^n) = v_{i-1/2}^n$$
 (32)

$$h_i^{-1}(s_i^n - s_{i-1}^n) = t_{i-1/2}^n$$
 (33)

$$(1-n)(v_{j}-v_{j-1}) + \frac{h_{j}}{4} \left(\frac{1+m}{2} + \alpha(1-m)\right) (f_{j} + f_{j-1})(v_{j} + v_{j-1}) + \frac{nWe}{2} (v_{j} + v_{j-1})(v_{j} - v_{j-1})$$

$$-(m-\alpha(1-m))\frac{h_{j}}{4} (u_{j} + u_{j-1})^{2} + mh_{j} + \frac{h_{j}}{2} \lambda \sin(\Omega)(s_{j} + s_{j-1}) - Ha \frac{h_{j}}{2} (u_{j} + u_{j-1})$$

$$-(1-m)\frac{\alpha h_{j}}{2} f_{j-1/2}^{n-1} (v_{j} + v_{j-1}) + (1-m)\frac{\alpha h_{j}}{2} v_{j-1/2}^{n-1} (f_{j} + f_{j-1}) = [R_{1}]_{j-1/2}^{n-1}$$

$$\frac{1}{\Pr} (t_{j} - t_{j-1}) + \frac{h_{j}}{4} \left(\frac{1+m}{2} + \alpha(1-m)\right) (f_{j} + f_{j-1})(t_{j} + t_{j-1}) - (1-m)\frac{\alpha h_{j}}{4} (u_{j} + u_{j-1})(s_{j} + s_{j-1})$$

$$+ \frac{\alpha h_{j}}{2} (1-m) s_{j-1/2}^{n-1} (u_{j} + u_{j-1}) - \frac{\alpha h_{j}}{2} (1-m) u_{j-1/2}^{n-1} (s_{j} + s_{j-1}) - \frac{\alpha h_{j}}{2} (1-m) f_{j-1/2}^{n-1} (t_{j} + t_{j-1})$$

$$+ (1-m)\frac{\alpha h_{j}}{2} t_{j-1/2}^{n-1} (f_{j} + f_{j-1}) = [R_{2}]_{j-1/2}^{n-1}$$

$$(35)$$

where we have used the abbreviations

$$\left[R_{1} \right]_{j-1/2}^{n-1} = -h_{j} \begin{bmatrix} (1-n)(v')_{j-1/2}^{n-1} + \left(\frac{1+m}{2} - \alpha (1-m) \right) (fv)_{j-1/2}^{n-1} + nWe(vv')_{j-1/2}^{n-1} \\ - (m-\alpha (1-m)) (u_{j-1}^{n-1})^{2} + \lambda \sin(\Omega) s_{j-1/2}^{n-1} - Ha u_{j-1/2}^{n-1} \end{bmatrix}$$
 (36)

$$[R_2]_{j-1/2}^{n-1} = -h_j \left[\frac{1}{\Pr} (t')_{j-1/2}^{n-1} + \left(\frac{1+m}{2} - \alpha (1-m) \right) (ft)_{j-1/2}^{n-1} + \alpha (1-m) (us)_{j-1/2}^{n-1} \right]$$
(37)

The boundary conditions are:

$$f_0^n = u_0^n = 0, s_0^n = 1, u_J^n = 0, s_J^n = 0$$
 (38)

Stage 3: Quasilinearization of Non-Linear Keller Algebraic Equations

If we assume $f_j^{n-1}, u_j^{n-1}, v_j^{n-1}, s_j^{n-1}, t_j^{n-1}$ to be known for $0 \le j \le J$, this leads to a system of 5J+5 equations for the solution of 8J+8 unknowns $f_j^n, u_j^n, v_j^n, s_j^n, t_j^n$, j=0,1,2,...,J. This non-linear system of algebraic equations is linearized by means of Newton's method.

Stage 4: Block-tridiagonal Elimination Solution of Linear Keller Algebraic Equations

The linearized system is solved by the block-elimination method, since it possess a blocktridiagonal structure. The bock-tridiagonal structure generated consists of block matrices. The complete linearized system is formulated as a block matrix system, where each element in the coefficient matrix is a matrix itself, and this system is solved using the efficient Keller-box method. The numerical results are strongly influenced by the number of mesh points in both directions. After some trials in the η -direction (radial coordinate) a larger number of mesh points are selected whereas in the ξ -direction (tangential coordinate) significantly less mesh points are utilized. η_{max} has been set at 8.0 and this defines an adequately large value at which the prescribed boundary conditions are satisfied. ξ_{max} is set at 3.0 for this flow domain. Mesh independence is achieved in the present computations. The numerical algorithm is executed in MATLAB on a PC. The method demonstrates excellent stability, convergence and consistency, as elaborated by Keller [45].

RESULTS AND DISCUSSION

Table 1 provides the shear stress rate (C_f) values for various m values. The existing findings are compared with Khan and Pop [51], Yacob et al. [52] and White [53] and are found to be in excellent correlation that supports the reliability of the current KBM code. Table 2 illustrates the impacts of We, n, m, γ , Ha and λ on C_f and Nu along with a variation in ξ . An increase in We is seen to enhance C_f whereas Nu is reduced. The parameter We defines the relative effect of viscous force to elastic force for flows. It is perhaps inversely or directly related to viscous force. Also, it characterizes the association between the fluid's stress relaxation time and the particular time of operation. In general, Weissenberg number arises from scaling the evolution of stress in rheological research and embedded within this are available alternatives for fluids with various

shear or elongation rate and length scales. From the def., $\textit{We}\left(\frac{\sqrt{2\nu\Gamma}\,\text{Re}_x^{3/2}}{x^2}\right)$ is directly proportional

to Time dependent material constant (Γ), fluid elasticity and inversely proportional to ν^{V2} . Hence the Weissenberg number is lowered for higher viscosity and as the velocity is decreased, this helps to maximize skin friction. As We reaches 0, the flow become Newtonian. It is further noted that with rising n values reduces C_f but enhance Nu. A rise in power law index induces the stream to differ from Newtonian flows and reduces the velocity and hence the shear stress also reduces. Also, rising m is found to enhance both C_f and Nu. A rise in γ is noted to enhance both C_f and Nu. It has been observed that a rise in λ enhance both C_f and Nu. There is a significant decline in C_f and Nu with higher Ha values (Ha represents relative influence of Lorentz's magnetic drag force to viscous hydrodynamic and buoyancy forces). A rise in magnetic drag force obviously prevents

the movement of boundary layer and allowing a retardation and a reduction in the skin friction. Hence, the momentum boundary layer thickness will be improved. Also, the thermal improvement coupled with an increase in magnetic field leads the fluid temperature to exceed the wall temperature that counteracts the heat transfer from wall to fluid body. Hence the heat transfer rate is essentially reduced.

Figs. 3 – 6 depicts the influence W_e on velocity (f'), temperature (θ) , entropy (Ng) and Bejan number (Be) profiles. A reduction in velocity is observed near-wall region, with rising We (fig. 3). The parameter We characterizes the association between the fluid's stress relaxation time and the particular time of operation. Hence for greater We values, the relaxation time is increased and hence the velocity decreases. There seems to be a low viscosity effect with greater We values and hence the flow is less deformable. The momentum development is hampered by tougher fluids (low elasticity) and the boundary layer is thickened due to the inverse relation between We and viscosity. However, such impact is not retained in the far field regime where the momentum diffusion is promoted with greater fluid relaxation and a week acceleration with higher We is induced. It can be intimately related to the alteration in tensile stresses in the structure of the rheological boundary layer when shifting from the near wall regime to the free stream regime. The effects of We is temperature consistent, while the velocity is turned over. Evidently, the rheology of the fluid is more closely related to the diffusion of momentum than to thermal diffusion. The latter is affected indirectly, i.e. by the primary influence of fluid viscoelasticity, which is a secondary effect. In the boundary layer, there is naturally a rivalry between elastic and viscous forces, which depends, among other variables, on the proximity to the wedge surface. In context of the evolution of temperature this is not clear. The presumption is that a consistent and uniform temperature distribution during the coating process should be achieved, regardless of the degree of elasticity of the liquid (e.g. spray paint). Indeed, as W_{ℓ} increases, the temperature distributions increase slightly (fig. 4) and hence the thermal thickness of the boundary layer also increases. Also in figs. 5 and 6, it is observed that Ng is increased slightly for greater We values whereas Be is lowered for greater We values. Physically, the relaxation time rises with larger We values implies that fluid particles resist more that results in loss in heat.

Figs. 7 – 10 illustrates the influence n on velocity (f'), temperature (θ) , Ng and Be profiles. The fluid velocity (Fig. 6) is significantly increased with increasing n. A rise in n values shortens the fluid's friction and hence the velocity is increased. For greater n values, the fluid

passes on to a viscous medium and leaves elastic properties. Hence the momentum diffusion is increased and hydromagnetic boundary layer thickness is reduced. Conversely, temperature, Ng and Be are reduced with a rise in n values. An increase in n values, steadily decreases temperature as momentum diffusion rate exceeds thermal diffusion rate resulting in cooling the boundary layer regime.

Figs. 11 – 14 presents the influence m on velocity (f'), temperature (θ) , Ng and Be profiles. It is reported with increasing m values, the velocity increased significantly while the temperature fell considerably. For increasing m values a huge rise in Ng and Be is observed. For m=0 in eqn. (10) the Blasius flow past a flat plate is achieved. The momentum boundary layer thickness is lowered efficiently with greater pressure gradient and the thermal boundary layer thickness is also reduced. With m=1, we obtain the case of flow on an infinite plate in the vicinity of the stagnation point flow. Although these two instances of flow are of mathematical interest, they are not in functional polymer production. For $m \neq 0$, the generalized wedge case is more important.

Figs. 15 – 18 depict the influence λ on velocity (f'), temperature (θ), Ng and Be profiles. With increasing λ values, a small rise in velocity is noted. By def., λ represents the ratio of buoyancy force to the viscous force. Greater λ values lead to improved natural convection. The viscous effect is less with greater λ values and hence velocity increases. Physically, greater λ values leads to increase in the convective cooling phenomenon and hence the fluid velocity increase. On the other hand, the fluid temperature is slightly reduced with increasing λ values which is due to the acceleration in the convective cooling phenomenon of the system. Fig. 17 reveals that there is an improvement in the Ng in near vicinity to the wedge surface with an increase in λ values, although there is a decline further from the wedge surface. Also for $\eta > 2$, the entropy converges asymptotically to zero. With increasing λ values, the Bejan number is significantly enhanced near the surface and reduced far from the surface. Nevertheless, the Bejan number profiles converse at an intermediate distance from the wedge surface, suggesting that there is no tangible effect of the mixed convection in this area.

Figs. 19 – 22 presents the influence γ on velocity (f'), temperature (θ) , Ng and Be profiles. With rising γ values, a very small change i.e. a small increase in velocity is observed. And with increasing γ values, a significant rise in temperature, Ng and Be is observed. A rise in Boit number increases the buoyancy force and the fluid carries the heat energy with higher velocity. Therefore, as γ increases, the velocity also increases. The fluid considered in the present study is incompressible with respect to pressure but not temperature. Therefore, the fluid density changes with temperature variation due to thermal expandability and the flow is influenced by the buoyancy force. Hence, as γ rises the temperature also rises. The entropy and Bejan numbers are also enhanced with a rise in Biot number. The regime is often reffered to as thermally simple for $\gamma < l$ and there is exists more consistent temperature fields within the boundary layer and solid wedge surface. The thermal fields are predicted to be nonlinear inside the solid wedge surface for $\gamma > l$. The Biot number essentially relates the conduction resistance inside a solid body to the convection resistance external to the body for heat transfer. It can also be observed that, $\gamma > 0.1$ refers to a thermally dense component, while a thermally thin component is indicated for $\gamma < 0.1$. By def, γ is inversely proportional to thermal conductivity, hence the thermal conductivity at the wedge surface will decrease as the biot number increases and this leads to a reduction in the heat transfer rate from the boundary layer to inside the wedge, exhibiting in an increase in temperature at the wedge surface and the maximum effect at the surface will be preserved in the fluid body.

Figs. 23 – 26 depict the influence Ω on velocity (f'), temperature (θ) , Ng and Be profiles. When the inclination angle increases, the velocity is seen to increase slightly while the temperature distribution is found to decrease slightly. Also, the entropy generation number is seen to enhance as the inclination angle rises while the Bejan number is slightly reduced with increasing inclination angle.

Figs. 27 –30 depict the influence Ha on velocity (f'), temperature (θ) , Ng and Ba profiles. Fig. 27 illustrates that the velocity profiles are depleted by increasing magnetic effects. Increasing the Ha values results in an improvement in the Lorentzian magnetohydrodynamic drag force. This Lorentz force reduces the shear effect on the wedge surface and thus decreases fluid velocity rapidly. The strong applied magnetic field resists the momentum flow which causes decline in the flow and thus increases the momentum boundary layer thickness. Alternatively, with an increase in Ha values, the temperature magnitudes are augmented slightly thereby increasing the thermal boundary layer thickness. Fig. 29 demonstrates that with an increase in Ha, a significant downfall in Ng is produced. The Bejan number is notably augmented with an increase in Ha values.

Figs. 31 – 34 illustrates the influence *Br* and *Re* on *Ng* and *Be* profiles respectively. The variations of *Br* on *Ng* and *Be* are illustrated in Figs. 31 & 32 respectively. It is obvious from fig. 31 that the *Ng* profiles are greatly increased with increasing Br and the impact is more pronounced near the wedge surface. Initially, the energy is produced due to the dragged Lorentz forces produced which increases the entropy of the fluid. The thermal conductivity of the fluid declines with the rising *Br*, so that a greater amount of heat is transmitted through the fluid. The parameter *Br* characterizes the heat generated by viscous dissipation. This results in an enhancement in the entropy generation. Conversely, the Bejan number is reduced with respect to *Br* which is due to the dominant influence of viscous irreversibilities compared with irreversibilities in heat transfer. Figs. 33 & 34 presents the distributions of *Ng* and *Be* for various values of *Re*. Both *Ng* and *Be* are increased with a rise in *Re* values. The inertial force dominates the flow with reduced viscous force and results in a significant contribution of heat transfer to the entropy. The Reynolds number and entropy generation are proportional to each other. The Bejan number is also seen to increase with increasing values of *Re*.

CONCLUSIONS

The entropy generation of mixed convection flows of tangent hyperbolic fluid past isothermal wedge is considered. The Keller's implicit finite difference numerical technique is used to solve the modified, non-dimensional governing equations, subject to practical boundary conditions effectively. Absolutely brilliant association with prior research testifying to validity of this code is illustrated. The second law thermodynamics analysis of the flow is conducted by adopting the Bejan's entropy generation minimization approach. The calculations showed that:

- An increase in We is seen to reduce velocity, Ng and Be whereas it elevates temperature.
- II. Increasing n increases the velocity whereas depresses temperature, entropy generation number and Bejan number.
- III. An increase in γ is seen to increase velocity, temperature, entropy generation number and Bejan number.
- IV. An increase in m is seen to increase velocity, Ng and Be but reduces the temperature.

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TABLES

Table 1: Comparison of the values of C_f for various values of m when $\lambda = 0$

m	Khan and	Yacob et	White	Present	
m	Pop [51]	al. [52]	[53]	results	
0	0.4696	0.4696	0.4696	0.4696	
1/11	0.6550	0.6550	0.6550	0.6549	
1/5	0.8021	0.8021	0.8021	0.8019	
1/3	0.9277	0.9276	0.9277	0.9275	
1/2	1.0389	1.0388	1.0389	1.0387	
0	1.2326	1.2326	1.2326	1.2324	

Table 2: Values of C_f and Nu for different W_e , n, m, γ , λ , Ha and ξ $(\Omega = 30^0, Pr = 7.0)$

$W_{\mathbf{e}}$	***	m	mλ	γ	На	ξ = 1.0		ξ = 2.0		$\xi = 3.0$	
We	n					C_f	Nu	C_f	Nu	C_f	Nu
0						0.4920	0.4431	0.4731	0.4357	0.4652	0.4327
0.5						0.5043	0.4386	0.4844	0.4315	0.4760	0.4286
2						0.5360	0.4284	0.5136	0.4215	0.5042	0.4188
3						0.5541	0.4230	0.5304	0.4163	0.5204	0.4136
5						0.5858	0.4144	0.5599	0.4079	0.5490	0.4053
	0					0.5893	0.4228	0.5667	0.4156	0.5573	0.4127
	0.25					0.5153	0.4370	0.4952	0.4298	0.4868	0.4269
	0.5					0.4356	0.4560	0.4151	0.4486	0.4079	0.4457
	0.75					0.3374	0.4827	0.3226	0.4753	0.3165	0.4725
	0.85					0.2947	0.4967	0.2809	0.4895	0.2753	0.4868
		0.1				0.2549	0.3197	0.2507	0.3191	0.2492	0.3191
		0.2				0.3242	0.3550	0.3173	0.3536	0.3144	0.3528
		0.3				0.3873	0.3870	0.3763	0.3832	0.3716	0.3814
		0.4				0.4454	0.4152	0.4298	0.4092	0.4234	0.4068
		0.5				0.4995	0.4404	0.4800	0.4331	0.4718	0.4302
			0			0.4692	0.4357	0.4491	0.4277	0.4407	0.4246
			2			0.5874	0.4540	0.5692	0.4481	0.5615	0.4458
			4			0.6989	0.4708	0.6818	0.4660	0.6746	0.4641
			6			0.8052	0.4860	0.7890	0.4819	0.7821	0.4803
			9			0.9572	0.5062	0.9419	0.5029	0.9355	0.5016
				0.3		0.4794	0.1458	0.4595	0.1432	0.4512	0.1422
				0.5		0.4995	0.4404	0.4800	0.4331	0.4718	0.4302
				1		0.5145	0.6641	0.4952	0.6536	0.4871	0.6493
				1.5		0.5194	0.7391	0.5002	0.7276	0.4922	0.7230
				2		0.5219	0.7768	0.5027	0.7647	0.4947	0.7599
					0	0.5503	0.4577	0.5312	0.4165	0.5232	0.4485
					0.05	0.5235	0.4489	0.5044	0.4246	0.4964	0.4392
					0.1	0.4995	0.4404	0.4800	0.4331	0.4718	0.4302
					0.15	0.4774	0.4323	0.4577	0.4419	0.4494	0.4216
					0.2	0.4574	0.4245	0.4374	0.4511	0.4290	0.4133

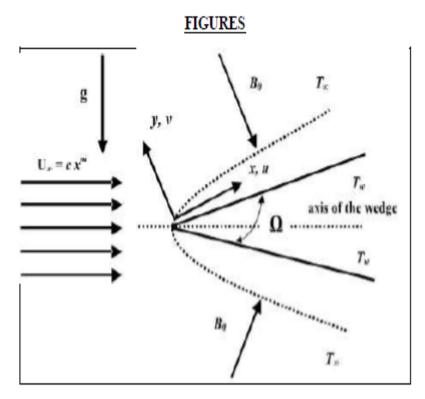


Fig. 1 Flow analysis along the wall of the edge

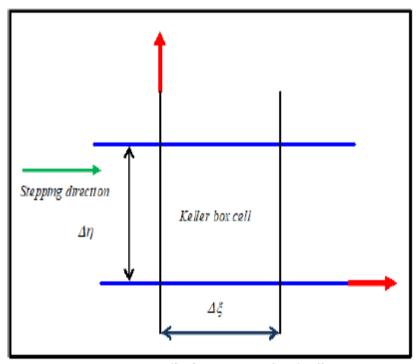


Fig. 2: Keller box computational cell

